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Important Instructions to examiners:

- 1) The answers should be examined by key words and not as word-to-word as given in the model answer scheme.
- 2) The model answer and the answer written by candidate may vary but the examiner may try to assess the understanding level of the candidate.
- 3) The language errors such as grammatical, spelling errors should not be given more Importance (Not applicable for subject English and Communication Skills.
- 4) While assessing figures, examiner may give credit for principal components indicated in the figure. The figures drawn by candidate and model answer may vary. The examiner may give credit for any equivalent figure drawn.
- 5) Credits may be given step wise for numerical problems. In some cases, the assumed constant values may vary and there may be some difference in the candidate's answers and model answer.
- 6) In case of some questions credit may be given by judgement on part of examiner of relevant answer based on candidate's understanding.
- 7) For programming language papers, credit may be given to any other program based on equivalent concept.



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Q No.	Answer	marks	Total marks
Q1 A	Attempt any six		12
a)	Catalyst used for sulfuric acid production	1 mark	2
	Platinum	each	
	Vanidium pentoxide		
b)	Oleum or fuming sulfuric acid , is a solution of various compositions of sulfur	2	2
	trioxide in sulfuric acid.		
c)	Reactions in sulfuric acid manufacturing	2	2
	$S + O_2 = SO_2$		
	$SO_2 + \frac{1}{2}O_2 = SO_3$		
	$SO_3 + H_2O = H_2SO_4$		
d)	Properties of sulfuric acid	½ each	2
	Molecular weight: 98	for any	
	Melting point 10.5 °C	two uses	
	• Boiling point 340°C with decomposition	and	
	Completely miscible with water with large heat of solution	propertie	
	• Formation of oleum with SO ₃	S	
	Uses of sulfuric acid		
	Production of phosphoric acid, Fetriliser, petroleum refining, concentration of		
	nitric acid.		
e)	Catalyst for ammonia production	2	2
	Iron promoted with K ₂ O, CaO, SiO ₂ , and Al ₂ O ₃		
f)	Cell notation for diaphragm cell		2



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	Anode Cathode	T	
	\uparrow Cl ₂ , C NaCl (aq) NaOH (aq) Fe, H ₂ \uparrow		
	Cell reaction :		
	Anode: $CI^ e^- \rightarrow \frac{1}{2} CI_2$		
	Cathode: $Na^{+} + H_{2}O + e \rightarrow Na^{+} + OH^{-} + \frac{1}{2} H_{2}$		
	Overall: NaCl + $H_2O \rightarrow NaOH + \frac{1}{2} H_2 + \frac{1}{2} Cl_2$		
g)	Water gas is a synthesis gas, containing carbon monoxide and hydrogen	2	2
h)	Gypsum	2	2
	CaSO ₄ ·2H ₂ O		
Q 1B	Attempt any two		8
a)	Nelson cell	4	4
	Brine H2 Asbestos diaphragm Perforated steel cathode Steam NaOH brine solution		
b)	Industrial Fuel Gases	1 mark	4
	1. Hydrogen : As a fuel, feed stock for ammonia, in petrochemical	each	
	2. Acetylene : As a fuel in oxy-acetylene flame, polymer		
	3. Water gas: As a fuel, as a source of hydrogen		
	4. Producer gas: As a fuel		



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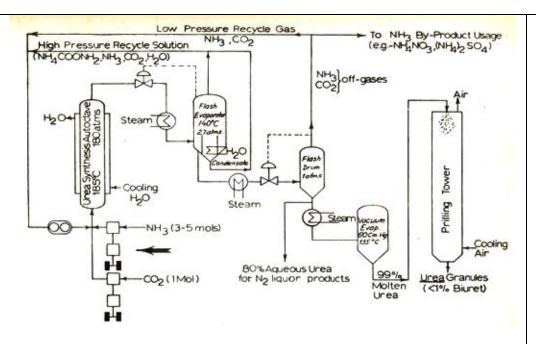
C	Cement				2	4
C	Cement is generic name for pow	dered material wh	ich initially have pla	stic flow		
w	when mixed with water but form	n a solid structure	in several hours with	varying		
d	egree of strength and binding p	roperties which co	ontinue to improve wi	ith age.		
P	ortland Cement				2	
	Compound	Formula	Shorthand form			
	Tricalcium aluminate	Ca ₃ Al ₂ O ₆	C ₃ A			
	Tetracalcium aluminoferrite	Ca ₄ Al ₂ Fe ₂ O ₁₀	C ₄ AF			
	Belite or dicalcium silicate	Ca ₂ SiO ₅	C_2S			
	Alite or tricalcium silicate	Ca ₃ SiO ₄	C ₃ S			
	Sodium oxide	Na ₂ O	N			
	Potassium oxide	K ₂ O	K			
	Gypsum	CaSO ₄ .2H ₂ O	CSH ₂			
2 A	Attempt any two					16
U	Jrea by Montecatini Process:				Rection-1	8
C	Chemical reaction:				Diagram-	
i) CO ₂ (carbon dioxide)	$+$ 2NH $_3$ (am	nmonia) \rightarrow NH ₄ .C	OO.NH ₂	4	
	(ammonium carbamate)				Process-3	
ii	i) NH ₄ .COO.NH ₂ (ammoni	um carbamate) →	NH ₂ .CO.NH ₂ (urea	$+ H_2O$		
ii	ii) Undesirable side reaction	n :				
	$NH_2.CO.NH_2$ (urea) $\rightarrow N$	NH ₂ .CO.NH.CO.N	JH_2 (biuret) + NH_3			
$ _{\mathrm{F}}$	low diagram :					

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Process description:

Ammonia and carbon dioxide are compressed separately and added to the high pressure autoclave which must be water cooled due to highly exothermic reaction. The average residence time in the autoclave, which is operated on a continuous basis, is $1.5\,$ to $2\,$ hrs. a mixture of urea, ammonium cabamate, water and unreacted NH $_3$ and CO $_2$ results.

This liquid effluent is let down to 27 atms and feed to a special flash evaporator containing gas liquid separator and condenser. unreacted NH₃, CO₂ and water as a solution are removed and recycled. An aqueous solution of carbamate urea is passed to the atmospheric flash drum where further decomposition of carbamate takes place. The off gases from this step can either be recycled or sent to ammonia process for making chemical fertilizers.

The 80% aqueous urea solution can be used as it is or sent to a vacuum evaporator to obtained molten urea containing less than 1% water. The molten

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3			Ü
	mass is them sprayed into prilling or granular solidification tower. To avoid		
	formation of biuret in percentage $> 1\%$, the temperature must be kept just		
	above the melting point for processing time of 1-2 seconds in this phase of the		
	operation.		
2-b	Phosphoric acid	2	8
	Reaction:		
	$Ca_3(PO_4)_2 + 3H_2SO_4 + 6H_2O = 2H_3PO_4 + 3(CaSO_4.2H_2O)$		
	Vent Gas Hot Wash Water Water To Gypsum Wash Gypsum Plant	3	
	Ground Phosphate Recycle H3PQ1 93.98% H2SQ Sludge Single Effect Evaporator Air Steam Steam T55% St		
	1Process:		
	Phosphate rock is ground and fed to chute where a recycle stream of weak		
	phosphoric acid washes into reaction tank. Strong sulfuric acid is fed to the		
	reactor. Around 98% conversion takes in 4-6 hours. Heat of reaction is		
	controlled by using cooling air. Gypsum -Acid slurry is fed to travelling pan		
	filter where 40% acid is removed and cake is washed with water. Filtrate is		
	return to the reactor. The gypsum obtained is dried and send for paint or cement		
	manufacturing. Dilute acid obtained can be concentrated in single effect	3	
	evaporator.		

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2.0	Manufacturing Process of coustic sade and ablaving	0	0
2-c	Manufacturing Process of caustic soda and chlorine Brine Brine	8	8
	Freon Salt Mercury cell To Constant Head feed tank Filter Denuding tower Cantriluge Constant Head feed tank Filter Denuding tower		
Q 3	Attempt any four		16
a)	Structure	1	4
	Yellow phosphorous		
	P 60° P		
	Red phosphorous		
	P P P P P P P P P P P P P P P P P P P	1	

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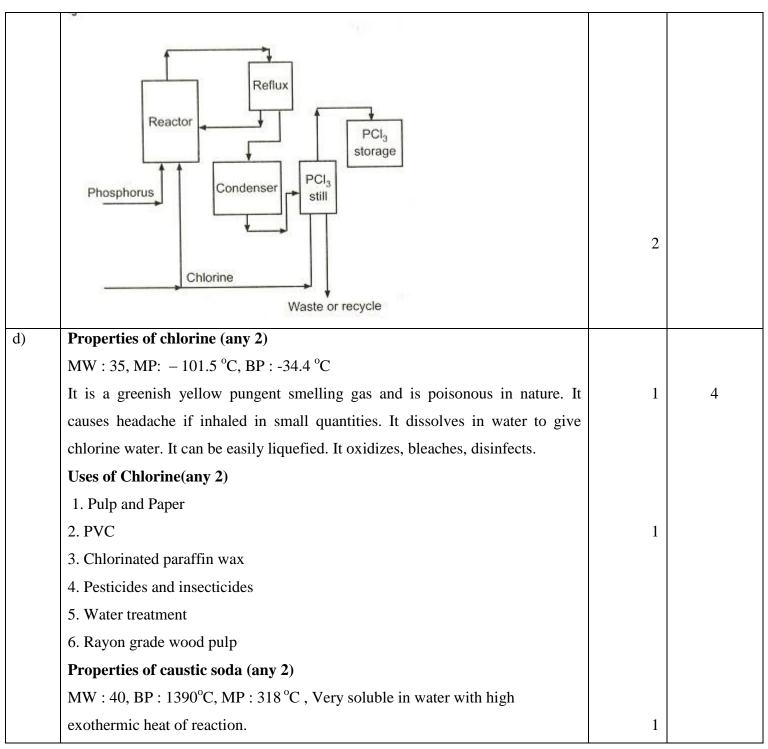
	Properties	2	
	MW =60		
	$MP = 44.1^{\circ}C$		
	$BP = 280 ^{\circ}C$		
	Stored under water due to reaction with oxygen.		
b)	Electro thermal process:	Rection-1	4
	A mineral phosphate with sand and coke is charged in the electric furnace. It is	Process-3	
	heated upto 1400 to 1500 °C.		
	Initially at 1150°C, SiO ₂ displace more volatile P ₂ O ₅ from calcium phosphate.		
	P ₂ O ₅ is then reducing to phosphorous by coke at 1500°C. following reaction		
	takes place		
	$Ca_3(PO_4)_2 + 3SiO_2 \rightarrow 3CaSiO_3 + P_2O_5$		
	$2P_2O_5 + 10C \rightarrow P_4 + 10CO$		
	CaSiO ₃ from molten slag is periodically removed through hole. Vapors of		
	Phosphorous and carbon monoxide are send to the tank where cold water is		
	placed. Phosphorous vapors are condensed to white phosphorous and carbon		
	monoxide is escaped.		
c)	Phosphorous trichloride is prepared by direct reunion of phosphorus and	2	4
	chlorine, the reaction being exothermic and spontaneous.		
	$P_4 + 6Cl_2 \longrightarrow 4 PCl_3$		
	Liquid phosphorous and chlorine gas are fed in reactor. PCl ₃ formed is partly		
	refluxed in the reflux and a part is passed through a condenser and then to a still		
	for distillation and finally for storage.		
	It is analyzed for elemental phosphorus. Based on this analysis, additional		
	chlorine is introduced to remove traces of unreacted phosphorus.		

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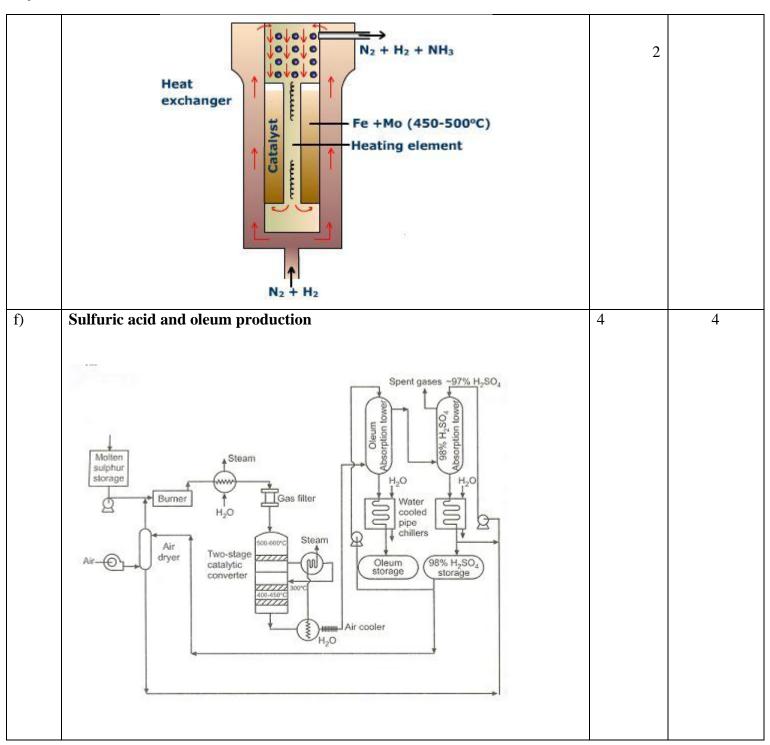
	Howard Counting and a (army 2)		
	Uses of Caustic soda (any 2)		
	1. Textile industry		
	2. Paper and Pulp		
	3. Alumina	1	
	4. Soap and detergent		
	5. Dyes		
e)	Ammonia converter.	2	4
	The gases enter the converter at the base and pass upward round the chamber		
	congaing catalyst Fe + Mo. Then they pass downward through the heat		
	exchanger. The heat exchanger contains several coils of pipe, the mixture of		
	gases get, heated by heat exchange and then passes downwards through the		
	central chamber. It contains heating element. The mixture of gases passes up		
	through the contact chamber congaing catalyst. Finally mixture of gases passes		
	out through the coils of pipe of heat exchanger. It gives most of the heat to the		
	fresh gases on their way to contact chamber. The proportion of ammonia in the		
	coming out from converter is about 10 to 20 % and is remixed by cooling the		
	mixture.		

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Q 4	Attempt any four		16
ı)	Synthesis process:		4
	The process generates hydrogen chloride by burning chlorine in a few percent		
	excess of hydrogen; chlorine and hydrogen are obtained as by products during		
	manufacture of caustic soda.		
	$H_2 + Cl_2 \longrightarrow 2 HCl$		
	Cold water added under control Hydrogen burning in chlorine Hydrogen Hydrogen	2	
	Dry hydrogen is made to burn in acid resisting burner fitted in a combustion chamber lined with silica bricks. Dry chlorine is passed into the combustion chamber when hydrogen burns in an atmosphere of chlorine to give HCl		
	The gas is passed through a cooler cooled by water spray and then through		
	absorber through which water flows down in controlled quantities.		
	The absorber is also cooled by a spray of cold water to remove the heat of	2	
	absorption of HCl in water. The solution of HCl flows into storage tank below.		
	An exhaust fan on the extreme right pumps out the waste gases which escape in		
	the atmosphere.		
)	Plaster of Paris, quick-setting gypsum plaster consisting of a fine white	2	4

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	powder (calcium sulfate hemihydrate), which hardens when moistened and		
	allowed to dry. Known since ancient times, plaster of paris is so called because		
	of its preparation from the abundant gypsum found near Paris.		
	Uses:	2	
	passive fire protection, as fireproofing products		
	Insulation		
	Filler in fertilizer		
	Decorative purpose		
c)	Single super phosphate	2	4
	Manufacturing of Single Super Phosphate is based on the simplest chemical		
	reaction amongst chemical fertilizers. The major raw materials required are		
	phosphate rock and sulphuric acid. The Rock Phosphate contains Tri Calcium		
	Phosphate which is insoluble in water and hence cannot be taken by the plant.		
	The Rock Phosphate is reacted with dilute Sulphuric Acid. The product of		
	reaction is Mono Calcium Phosphate which is soluble in water. This soluble		
	phosphate can be easily consumed by the plants.		
	Rock phosphate is ground very fine (93% passing through 100 mesh). The		
	measured / weighed quantity of Rock phosphates is fed into lead lined mixer,		
	where it is neutralized with dilute sulphuric acid. The reaction is very fast in the		
	beginning and the material is fine slurry which thickens quickly. The material is		
	discharged in the den where the material slowly solidifies. The den discharge is		
	fitted with den cutter which cuts the solid cake to powder. The Fluorine based		
	gases are liberated which are sucked by ID fan and scrubbed in multi stage		
	conventional scrubbers &venturi Scrubbers. The material gets cured in a few		
	days time.		
	Reaction		
	$[Ca_3(PO_4)_2]_3CaF_2 + 7H_2SO_4 = 3CaH_4(PO_4)_27CaSO_4 + 2HF$		
L		L	1

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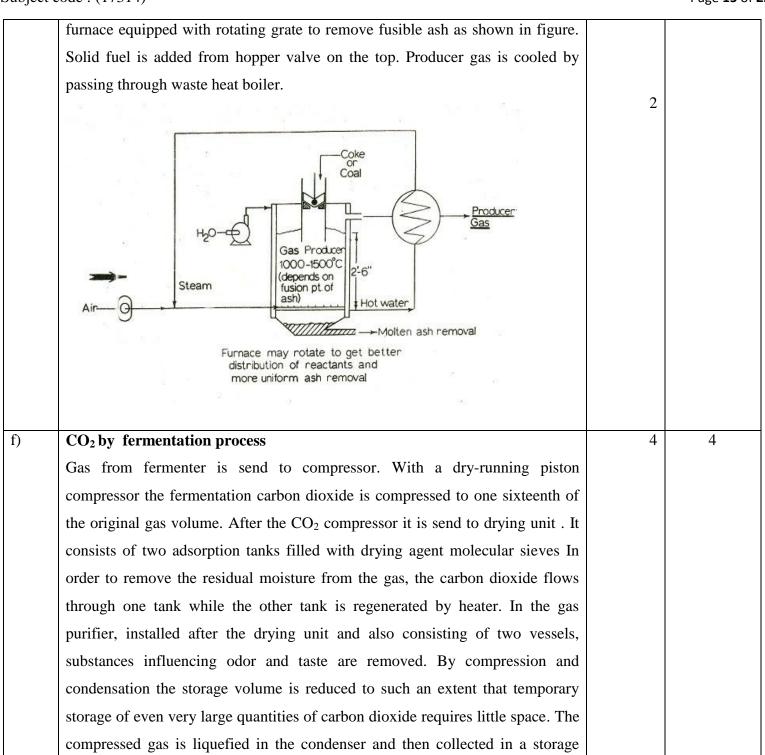
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	Phosphate rock Cyclone 60% H ₂ SO ₄ Ring roll mill Superphosphate SiO ₂ H ₂ O Rotary cylinder Rotary dryer	2	
d)	Fertilizer is any organic or inorganic material of natural or synthetic origin	2	4
	(other than liming materials) that is added to soil to supply one or more plant		
	nutrients essential to the growth of plants. Mined inorganic fertilizers have been		
	used for many centuries, whereas chemically synthesized inorganic fertilizers		
	were only widely developed during the industrial revolution.		
	Inorganic fertilizers		
	1. Nitrogen fertilizer: Urea, Ammonium nitrate, Ammonium sulphate,		
	Ammonium phosphate	2	
	2. Phosphorous fertilizer: Single superphosphate, Triple super phosphate		
	3. Potassium fertilizer : Potassium chloride, Potassium		
	sulphate		
e)	Producer gas, mixture of flammable gases (principally carbon monoxide and	2	4
	hydrogen) and nonflammable gases (mainly nitrogen and carbon dioxide) made		
	by the partial combustion of carbonaceous substances, usually coal, in an		
	atmosphere of air and steam.		
	Steam and air mixture injected in the bottom of water cooled jacket steel		

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	tank		
Q5	Attempt any two		16
a)	Solvay process	Rection-2	8
	The overall reaction can be regarded as between calcium carbonate and	Diagram-	
	sodium chloride:	3	
	CaCO ₃ + 2NaCl → CaCl ₂ + Na ₂ CO ₃	Process-3	
	However, calcium carbonate is too insoluble to react with a solution of salt.		
	Instead the product is obtained by a series of seven stages.		
	CO ₂ ,N ₂ to brine purifier		
	Cooling water		
	Purified (f) H ₂ O Flue gas		
	Purified brine solution Purified brine solution Purified brine solution CO2 Fuel + air H ₂ O Fuel + air H ₂ O Water Water		
	E (A)		
	(e) (g) Water cooler cooler		
	NH, recycle 0.5 kg/kg H₂O CO, 0 Soda ash		
	Coke		
	Lime stone CO ₂ Recycle NH ₃		
	Lime kiln (b) (c) Make-up NH ₃		
	H ₂ O Slakef (d) Milk of lime		
	Waste CaCl ₂ , impurities		
	The process is known as the ammonia-soda process or the Solvay process,		
	named after the Belgian industrial chemist who patented it in 186I. The		
	various stages of the Solvay process are interlinked as can be seen from the		
	diagram and description below.		
	diagram and description below.		

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(1) Ammoniation of brine

Ammonia gas is absorbed in concentrated brine to give a solution containing both sodium chloride and ammonia. Na⁺(aq), Cl⁻(aq), NH₄⁺(aq), OH⁻(aq) ions and NH₃(aq) are present.

(2) Formation of calcium oxide and carbon dioxide

Kilns are fed with a limestone/coke mixture (13:1 by mass). The coke burns in a counter-current of pre-heated air:

$$C(s) + O_2(g) \longrightarrow CO_2(g)$$
 $\Delta H^{\oplus} = -393 \text{ kJ mol}^{-1}$

The heat of combustion raises the temperature of the kiln and the limestone decomposes:

$$CaCO_3(s)$$
 \rightleftharpoons $CaO(s) + $CO_2(g)$ $\Delta H^{\oplus} = +180 \text{ kJ mol}^{-1}$$

The gas, containing approximately 40% carbon dioxide, is freed of lime dust and sent to the carbonating (Solvay) towers. The residue, calcium oxide, is used in ammonia recovery (see step 7 below).

(3) The Solvay Tower

This is the key stage in the process. The ammoniated brine from step (1) is passed down through the Solvay Tower while carbon dioxide from steps (2) and (5) is passed up it. The Solvay Tower is tall and contains a set of mushroom-shaped baffles to slow down and break up the liquid flow so that the carbon dioxide can be efficiently absorbed by the solution. Carbon dioxide, on dissolving, reacts with the dissolved ammonia to form ammonium hydrogencarbonate:

$$NH_3(aq) + H_2O(I) + CO_2(g) \longrightarrow NH_4HCO_3(aq)$$

The solution now contains ions Na⁺(aq), Cl⁻(aq), NH₄⁺(aq) and HCO₃⁻ (aq). Of the four substances which could be formed by different

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combinations of these ions, sodium hydrogencarbonate (NaHCO₃) is the least soluble. It precipitates as a solid in the lower part of the tower, which is cooled. The net process is:

$$NaCI(aq) + NH_3(aq) + H_2O(I) + CO_2(g) \longrightarrow NaHCO_3(s) + NH_4CI(aq)$$

A suspension of solid sodium hydrogencarbonate in a solution of ammonium chloride is run out of the base of the tower.

(4) Separation of solid sodium hydrocarbonate

The suspension is filtered to separate the solid sodium hydrogencarbonate from the ammonium chloride solution, which is then used in stage (7).

(5) Formation of sodium carbonate

The sodium hydrogencarbonate is heated in rotating ovens at 450 K so that it decomposes to sodium carbonate, water and carbon dioxide:

$$2NaHCO_3(s) \longrightarrow Na_2CO_3(s) + H_2O(g) + CO_2(g)$$

The carbon dioxide is sent back to the Solvay Tower for use in step (3). The product of the process, anhydrous sodium carbonate, is obtained as a fine white powder known as light sodium carbonate.

(6) Formation of calcium hydroxide

The last two stages, (6) and (7), are concerned with the regeneration of ammonia from ammonium chloride (made in step 3). The quicklime from step (2) is slaked with excess water giving milk of lime:

$$CaO(s) + H2O(I) \longrightarrow Ca(OH)2(aq/s)$$

(7) Regeneration of ammonia

This calcium hydroxide suspension is mixed with the ammonium chloride solution left from step (4) and heated:

$$2NH_4CI(aq) + Ca(OH)_2(aq/s) \longrightarrow CaCI_2(aq) + 2NH_3(g) + 2H_2O(I)$$

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		_
The ammonia is thus recovered, and sent back to step (1). Calcium chloride		
is the only by-product of the whole process.		
The overall process is an elegant one. In theory, the only raw materials are		
limestone and brine. Inevitably, there are losses of ammonia, and these are		
made up for by addition of extra supplies, as required in step (1)		
Nitric Acid Production	Rection-2	8
Raw material	Diagram-	
Ammonia, air, water	3	
Reaction	Process-3	
$4NH_3+5O_2 = 4NO + 6H_2O$		
$2NO+O_2 = 2NO_2$		
$3NO_2+H_2O=2HNO_3+NO$		
Ammonia and air are compressed and send to the catalytic converter. Ammonia is oxidized and converted into nitric oxide. Large heat is evolved which can de utilized to run turbine by producing steam and gas expander. Both are connected to the compressor. Hence compressor does not require external		



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	energy source. NOx gases after heat recovery is send through cooler condenser		
	where it is cooled by cooling tower water. Some part of acid is converted into		
	liquid form. Both liquid and gas are send to absorption tower at different feed		
	plates. Air is provided from the bottom to complete oxidation of NO. Water is		
	fed from the top of the tower. Nitric acid (60%) is collected at the bottom. Tail		
	gases from the absorber are used to run gas expander after heating.		
c)	CLAUDES PROCESS:		8
	Principle: when a cooled compressed gas is allowed to some external work e.g.	2	
	pushing the piston of gas engine, it falls in temperature.		
	Flow diagram:		
	Process description: Air freed from CO ₂ is dried, compressed and passes through a pipe surrounded by cold oxygen and nitrogen, where it is cooled. Cooled and compressed air is allowed to do work in an expansion engine where it is further cooled. This cooled air enters the plant and rises through iron tubes surrounded by	3	



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aoject	(1/31)		. 486 == 0
	liquid oxygen. a part of the air gets liquefied and collects. the condensation is	3	
	50% N2,50%O2 .the gas which escape condensation passes downwards through		
	side tubes surrounded by liquid oxygen and condenses. The condensation		
	being 99% N ₂ and 1% O ₂		
	The condensed liquid is pumped to the top of fractionating column, while the		
	bottom liq. Is pumped to a level slightly above the fractionating column, where		
	it meets an upward current of gases. the liq is wormed up a little as it comes		
	down and loses a volatile constituents more and more. i.e. N ₂ bye evaporation		
	and gets gradually richer in O ₂ . similarly up going gases loses more and more		
	O_2 by condensation due to cooling and gets richer in N_2 .by the time gases rich		
	the top, it is 99% pure N ₂ which escape to the exit provided. Liq O ₂ evaporate		
	as it cools the air and escape to the exit indicated		
Q6	Attempt any four		16
a)	Acetylene from CaC ₂	Mark	4
	Raw materials: lime stone, coke, water	should be	
	Chemical reactions:	given for	
	$CaO + 3C \longrightarrow CaC_2 + CO$	any	
	$CaC_2 + H_2O \longrightarrow Ca(OH)_2 + CH = CH$ $CaCO_3 \longrightarrow CaO + CO_2$	method	
	$2\text{CO} + \text{O}_2 \rightarrow 2\text{ CO}_2$		
	Process Description: Calcium carbide is produced by heating lime and coke in an electric furnace at	1	
	2100 °C . Molten CaC ₂ is solidified and cooled and ground under nitrogen	1	
	In the wet process the pulverized carbide is fed through a gas tight hopper to a		
	C2H2 generator in which the quality of water used is sufficient to discharge		
	Ca(OH) ₂ . The carbide is fed to water at a measured rate until exhausted.	2	
	Calcium hydroxide slurry containing 90% water is discharged. The gas is	3	
	passes through a scrubber to remove impurities like NH ₃ , sulphides, phosgene		

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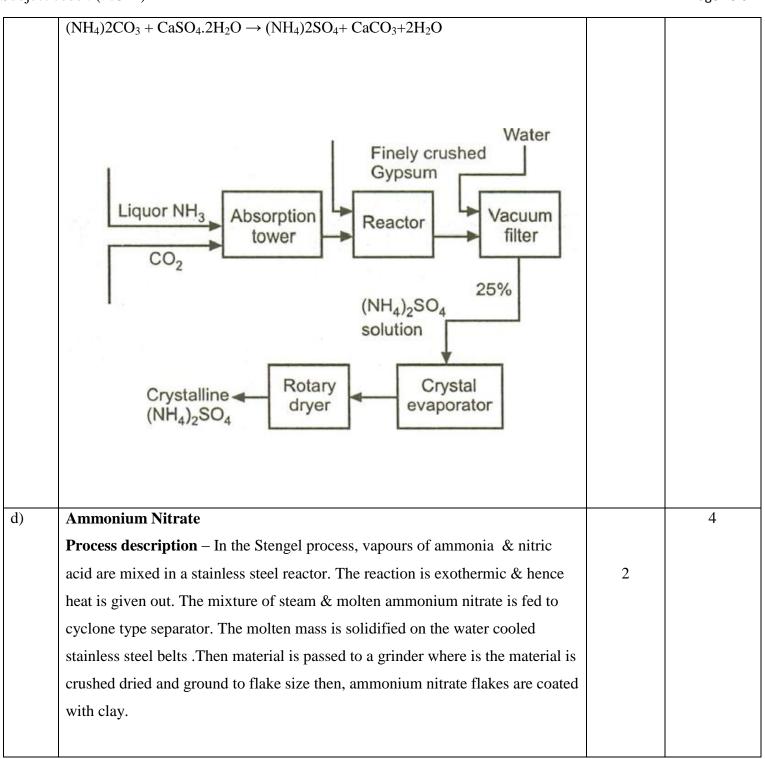
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	$2NH_3 + CO_2 + H_2O \rightarrow (NH_4)_2CO_3$		
c)	Ammonium sulfate	4	4
	in this process		
	Subsequent innovations allow for ash content >30% so Indian coal can be used		
	self-sustaining reaction of approximately zero heat release.		
	The correct ratio of steam, oxygen and coal is added to the reactor to yield a		
	separation procedure.	2	
	This process is based on use of tonnage or low purity grade oxygen made by air		
	This process was invented in 1940 by Germans.		
	Process description:		
	$C + H_2O \longrightarrow CO + H_2$		
	$C + O_2 \longrightarrow CO_2$	2	
	Reactions:		
	Raw materials: Steam, coal, oxygen		
b)	Water Gas (continuous process):		4
	of water pressure.		
	violently at 650°C. Hence temperature is maintained below 150°C and 30 cm		
	generator. Acetylene polymerizes at 250°C and above and decomposes		
	The dry process is more dangerous because of the temperature control in the		
	dry state.		
	reaction is largely dissipated by water vaporization leaving by product lime in		
	generator to eliminate waste disposal problem of lime slurry. The heat of		
	In a dry process equal weights of the quantities H ₂ O and CaC ₂ are used in the		
	atm.		
	The temperature in the gas generator is kept below 90°C and a pressure of 2		
	and finally through a purifier containing iron oxide and alumina or silica gel.		

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	Preheated HNO ₃ H ₂ O Cooling chamber Reactor and Sepqrator Cooler Cooling chamber Coating drum Product	2	
e)	Phosphorous	1	4
	Raw material:		
	Phosphate rock, coke, sand		
	Reaction:		
	$2Ca_3(PO_4)_2 + 10C + 6SiO_2 = P_4(Yellow) + 6CaSiO_3 + 10CO$		
	P_4 (Yellow) + heating = P_4 (Red)		
	Phosphate rock is ground, mixed with portion of coke requirement, then		
	sintered into nodules to obtain better electrical resistivity characteristics and to		
	avoid entrainment of fines in the released phosphorous and carbon monoxide	3	
	vapors. Screening is necessary to maintain size control with fines recycled to		
	the sintering operation. Coke breeze and sand particles are mixed in controlled		
	quantities based on phosphate rock analysis.		
	The electrical 3 phase furnace is at 230-300V designed with power fed to 100-		
	150cm diameter carbon electrode on each phase. The feed charge drops		
	gradually into the fused section of the furnace at 1400°C where the reduction to		
	elemental phosphorous takes place. The furnace is kept under slight vacuum by		
	fans in the downstream end of the plant, so the furnace gases moves to		

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	electrostatic precipitator to remove dust and then water cooled condenser.		
	Liquid yellow phosphorous is collected under water. CO obtained is used as		
	fuel. Molten slag obtained from furnace can be used as raw material for		
	furnace.		
f)	Dry process for Portland cement:		4
	The dry process is used when the raw material is either cement rock or blast	2	
	furnace slag. The calcareous raw material and argillaceous are crushed		
	separately by jaw or roller crusher(primary crushing) The material is dumped		
	to huge bins The raw material is mixed by automatic weighing machines then it		
	is fed to grinding mill, pulverized then to rotary kiln . Rotary kiln is 50-80m		
	long and having three times diameter kiln is inclined and rotate one revolution		
	per minute. Temperature maintained in the kiln is 1400-1500° C . The product		
	obtained is known as clinker removed from the lower end of the kiln then		
	ground with 2% gypsum to obtained Portland cement.		
	Calcareous materials Jaw Crusher Jaw Crusher Bin Mixing pulverizing Portland Clinker grinding	2	